

OF 1-CHLOROBUTANE BY DENYDRATED BACTERIA IN A CONTINUOUS SOLID-GAS BIOFILTER

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Abstract: *Rhodococcus erythropolis* NCIMB 13064 and *Xanthobacter autotrophicus* GJ10 are able to catalyze the conversion of halogenated hydrocarbons to their corresponding alcohols. These strains are attractive biocatalysts for gas phase remediation of polluted gaseous effluents because of their complementary specificity for short or medium and for mono-, di-, or trisubstituted halogenated hydrocarbons (C₂-C₈ for *Rhodococcus erythropolis* and C₁-C₄ for *Xanthobacter autotrophicus*).

After dehydration, these bacteria can catalyze the hydrolytic dehalogenation of 1-chlorobutane in a nonconventional gas phase system under a controlled water thermodynamic activity (a_w). This process makes it possible to avoid the problems of solubility and bacterial development due to the presence of water in the traditional biofilters.

In the aqueous phase, the dehalogenase activity of *Rhodococcus erythropolis* is less sensitive to thermal denaturation and the apparent Michaelis-Menten constants at 30°C were 0.4 mM and 2.40 $\mu\text{mol min}^{-1} \text{g}^{-1}$ for K_m and V_{max} , respectively. For *Xanthobacter autotrophicus* they were 2.8 mM and 0.35 $\mu\text{mol min}^{-1} \text{g}^{-1}$.

In the gas phase, the behavior of dehydrated *Xanthobacter autotrophicus* cells is different from that observed with *Rhodococcus erythropolis* cells. The stability of the dehalogenase activity is markedly lower. It is shown that the HCl produced during the reaction is responsible for this low stability. Contrary to *Rhodococcus erythropolis* cells, disruption of cell walls does not increase the stability of the dehalogenase activity.

The activity and stability of lyophilized *Xanthobacter autotrophicus* GJ10 cells are dependant on various parameters. Optimal dehalogenase activity was determined for water thermodynamic activity (a_w) of 0.85. A temperature of 30°C offers the best compromise between activity and stability. The pH control before dehydration plays a role in the ionization state of the dehalogenase in the cells. The apparent Michaelis-Menten constants K_m and V_{max} for the dehydrated *Xanthobacter autotrophicus* cells were 0.07 (1-chlorobutane thermodynamic activity) and 0.08 $\mu\text{mol min}^{-1} \text{g}^{-1}$ of cells, respectively.

A maximal transformation capacity of 1.4 g of 1-chlorobutane per day was finally obtained using 1g of lyophilized *Xanthobacter autotrophicus* GJ10 cells. © 2005 Wiley Periodicals, Inc.

Keywords: bioremediation; haloalkane dehalogenase; *Rhodococcus erythropolis* NCIMB 13064; solid-gas biofilter; waste air treatment; *Xanthobacter autotrophicus* GJ10

INTRODUCTION

Man-made halogenated volatile organic compounds (VOCs) are widely used as solvents and starting materials for the production of paints, agrochemicals, and pharmaceuticals. Due to their persistence and toxicity in the environment and their use in both industry and the home, they may cause considerable environmental pollution and human health problems (Mohn and Tiedje, 1992).

Although there is as yet no precisely international defined legal limit for halogenated VOC emissions, industrialized countries have made air quality a priority. Thus, these compounds are quoted by the U.S. Environmental Protection Agency (EPA) as priority environmental toxic pollutants (U.S. EPA, 1990). In this context, different methods of air treatment based on the physicochemical properties of the pollutant have been developed. One of these methods, biological waste air treatment, is both innovative and inexpensive.

Since they were first used in industry at the end of the 1970s, biological processes in waste air treatment have become increasingly common. The principle of waste air biotransformation is based on the oxidation of organic compounds by microorganisms. This biotechnological approach is an alternative technique that can supply reliable, simple and cheap technologies for air pollutant control (Belkin, 1992; Hardman, 1991).

Several research groups have dealt with some strains capable of hydrolytic dehalogenation of haloaliphatic compounds. The physiology, biochemistry, and genetics of dehalogenating bacteria and substrates specificity of their enzymes are currently being studied (Damborsky et al.,

2001; Hardman, 1991; Janssen, 2004; Janssen et al., 2001, Keuning et al., 1985; Kocabigik, 1989; Nagata et al., 1997).

In particular, a bacterium named *Xanthobacter autotrophicus* GJ10 is able to use a number of halogenated short-chain hydrocarbons and halogenated carboxylic acids as its sole carbon source for growth (Janssen et al., 1984). This microorganism constitutively produces a haloalkane dehalogenase that converts halogenated alkanes to their corresponding alcohol without the requirement of a coenzyme or oxygen (Shanstra et al., 1996).

The purified haloalkane dehalogenase isolated from *Xanthobacter autotrophicus* GJ10 catalyzes the hydrolytic dehalogenation of halogenated C₁ to C₄ alkanes, including chlorinated, brominated, and iodinated compounds (Keuning et al., 1985).

Many studies have focused on solid–liquid–gas biofilters using *Xanthobacter autotrophicus* GJ10 (Ferreira Jorge and Livingston, 2000; Reij and Hartmans, 1996) but there have been no reports on its use in other waste air biological treatment processes such as in nonconventional media. Recently, we have described the ability of dehydrated *Rhodococcus erythropolis* NCIMB 13064 cells to transform halogenated alkanes to their corresponding alcohol and HCl in a solid–gas biofilter (Erable et al., 2004, 2005). The solid–gas biofilter presents numerous advantages over the standard solid–liquid–gas biofilter: (a) there are no problems with the solubility of substrates and/or the products; (b) diffusion in the gaseous phase is more efficient than in solution, making mass transfers more efficient; (c) biomass development is not limiting since the dehydrated cells can't grow; (d) no addition of expensive nutrients is required to maintain cell viability (Lamare and Legoy, 1993).

The strains of *Rhodococcus erythropolis* NCIMB 13064 and *Xanthobacter autotrophicus* GJ10 have a different affinity for various substrates. For example, the 1,2-dichloroethane, natural substrate of *Xanthobacter autotrophicus* GJ10, is only slightly transformed by *Rhodococcus erythropolis* NCIMB 13064 (Schindler et al., 1999). The final goal of this new process is to carry out an association of bacteria able to convert a mixture of pollutants. In this context, the study of *Xanthobacter autotrophicus* GJ10 in the gas phase is essential to be able to treat dehalogenated short hydrocarbons.

Our purpose in this study was to investigate the ability of *Xanthobacter autotrophicus* GJ10 to transform 1-chlorobutane in a continuous solid–gas biofilter. The behavior of this strain is compared to that obtained with *Rhodococcus erythropolis* NCIMB 13064.

MATERIALS AND METHODS

Microorganisms, Culture Conditions, and Chemicals

The bacterial strain of *Xanthobacter autotrophicus* GJ10 was a gift from D.B. Janssen's research team, Department of Biochemistry, Groningen Biotechnology Center, Univer-

sity of Groningen, The Netherlands. *Xanthobacter autotrophicus* GJ10 was grown in 1-L aerobic flasks containing 200 mL of Luria Bertani (LB) medium at pH 7.0. The LB medium had the following composition (g/L): 10.0 tryptone, 5.0 yeast extract, and 5.0 NaCl. The medium was sterilized by autoclaving for 15 min at 121°C.

Rhodococcus erythropolis NCIMB 13064 was obtained from the National Collection of Industrial and Marine Bacteria LTD, Aberdeen, Scotland. The organism was grown in 1-L Erlenmeyer flasks sealed with Teflon-lined screw caps; the flasks contained 200 mL of a medium described by Sorkhoh et al. (1991) at pH 7.0. After cooling, 100 µL of filtered sterilized 1-chlorobutane was added twice as sole carbon source.

Both bacterial cultures were incubated at 30°C on an orbital shaker (160 rpm). Cell growth was monitored by measuring the optical density at 690 nm. After 48 h of growth, cells were harvested by centrifugation at 8000 rpm for 10 minutes.

All substrates were purchased from Sigma Co. (St. Louis, MO) except tryptone and yeast extract, which were obtained from Fluka (USA). Deionized water was obtained via a Milli-Q system (Millipore, France).

Preparation of Cells

Cells grown for 48 h were harvested by centrifugation (8000 rpm for 10 min), washed with 50 mM Tris/HCl buffer at pH 8.4 (*Xanthobacter autotrophicus*) and at pH 9.0 (*Rhodococcus erythropolis*) and resuspended in 50 mM Tris/HCl buffer at the same pH. Part of the cellular suspension was freeze-dried and used for 1-chlorobutane conversion tests in a solid–gas biofilter while the other part was used to measure the haloalkane dehalogenase activities of resting cells in aqueous phase.

Cell Disruption

The bacteria were disrupted by treatment with lysozyme (obtained from Sigma Chemical Co., St. Louis, MO) or by ultrasonic disruption. 200 mg of lysozyme were added to 600 mg of harvested cells that had been washed and resuspended in 30 mL of Tris/HCl buffer (50 mM at pH 8.4 or 9.0 for *Xanthobacter autotrophicus* GJ10 and *Rhodococcus erythropolis* NCIMB 13064, respectively). After 15 min incubation at 30°C, part of the preparation was frozen at –20°C and lyophilized. Alternatively, the cells were subjected to sonication treatment for a time period of between 0 and 10 minutes with a Vibra cell 72434 (Bioblock Scientific) at 50 W and a frequency of 20 kHz.

Enzyme Assay for Dehalogenation in the Aqueous Phase

The haloalkane dehalogenase activity of resting cells was assayed at 30°C in 50 mM Tris HCl buffer (pH 8.4 or 9.0). Tests were performed with 50 mL of cell suspension (in

Tris/HCl buffer) in 100-mL bottles. One hundred microliters of 1-chlorobutane were added and the reaction was stopped by centrifugation. One milliliter samples of the supernatant were removed and assayed for butan-1-ol levels by gas chromatography analysis using 1-hexanol as an internal standard and the same analytical conditions as for the analysis of the gas phase exiting the reactor.

Enzyme Assay for Dehalogenation in the Solid-Gas Biofilter

The solid-gas biofilter used in this study was described previously by Lamare and Legoy (1995). It consists of a 9-cm long glass tube in which the lyophilized *Xanthobacter autotrophicus* GJ10 cells are packed between two layers of glass wool. Substrate feeding was obtained by flowing nitrogen, used as a carrier gas, through the substrate saturation flasks. Substrates were continuously passed through the biofilter and reacted with the lyophilized *Xanthobacter autotrophicus* GJ10 cells. The gas leaving the biofilter was analyzed by gas chromatography. The acquisition and control of the operating parameters (substrate thermodynamic activity, water thermodynamic activity (a_w), temperature, and pressure) were monitored on line as shown in Figure 1.

The thermodynamic activity of each compound (X) in the reactor was calculated as follows:

$$a_x = \frac{Pp_x}{Pp_x^{Sat}}$$

with Pp_x the partial pressure of compound X in the gas entering the biofilter and Pp_x^{Sat} the saturation vapor pressure of pure compound X (atm) at the operating temperature.

The vapor phase leaving the biofilter was sampled using a 250- μ L loop on a six-way valve (Valco) maintained at

190°C. Samples were automatically injected into the split injector of a gas chromatograph.

A typical test was carried out at 30°C, with 100 mg of dehydrated cells. The total flow passing into the biofilter was 500 μ mol min^{-1} , the 1-chlorobutane thermodynamic activity (a_{clbut}) and the water thermodynamic activity (a_w) were fixed at 0.12 and 0.8, respectively. With these experimental conditions, less than 5% of substrate was transformed. These values were expressed in μ moles of butan-1-ol per minute and per gram of cells.

Chromatographic Analysis

Analyses were performed on a gas chromatograph (Hewlett Packard model 5890 A), equipped with a flame ionization detector (FID). The column used was an OV 1701 fused silica capillary column (25 m \times 0.25 mm i.d. \times 0.25 μ m film thickness; Chrompack, France). The split ratio was 43.2/2.7. The injector was kept at 200°C, and the detector was kept at 250°C. The column temperature was held at 40°C for 2.5 min, then programmed to increase at 15°C min^{-1} to 110°C and kept for 1 min at this temperature. Nitrogen was used as a carrier gas and the flow rate in the column was 2.7 mL min^{-1} . Hydrogen and air were supplied to the FID at 38 and 398 mL min^{-1} , respectively. Quantitative data were obtained after integration on a HP 3396A integrator.

RESULTS AND DISCUSSION

Dehalogenase Activities in the Aqueous Phase

The expression of dehalogenase activity in resting *Xanthobacter autotrophicus* GJ10 cells in the aqueous phase was

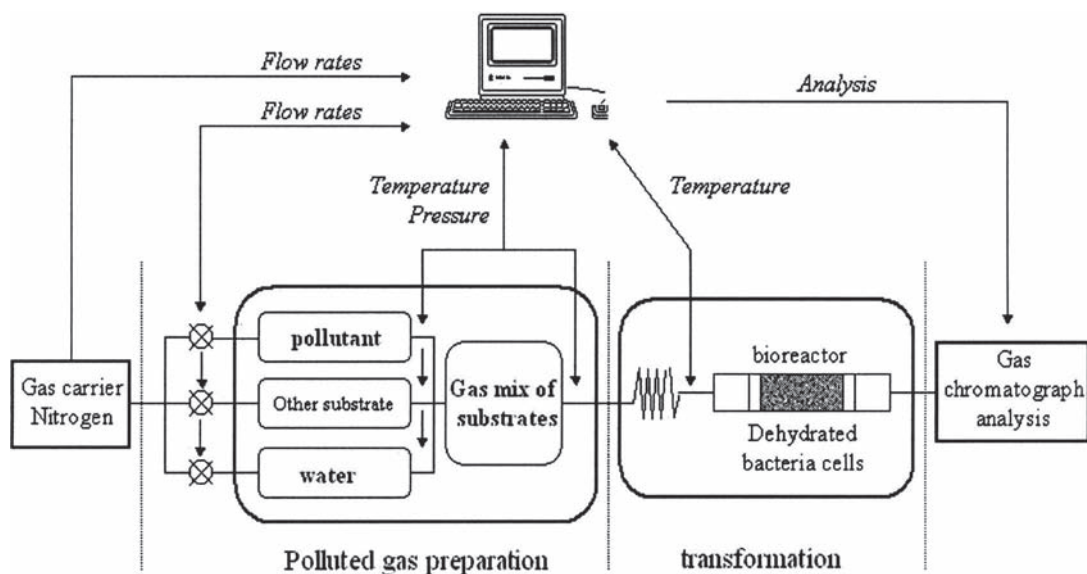


Figure 1. Schematic representation of the nonconventional gas phase biofilter.

first studied and compared to that of *Rhodococcus erythropolis* NCIMB 13064. Cells of *Xanthobacter autotrophicus* GJ10 grown on a nutrient media were harvested and used to carry out the irreversible hydrolysis of 1-chlorobutane to 1-butanol and HCl. The effect of several parameters such as temperature, buffer pH, buffer concentration, or substrate concentration was investigated. As shown in Table I, the maximum dehalogenase activity of *Xanthobacter autotrophicus* GJ10 cells was obtained at pH 8.4 and at 30°C. This dehalogenase activity was very sensitive to temperature and became rapidly inactive at temperatures over 40°C. Data on the free purified haloalkane dehalogenase of *Xanthobacter autotrophicus* GJ10 showed that the maximum dehalogenase activity was obtained at pH 8.2 and at a temperature of 37°C (Keuning et al., 1985). The optimal Tris/HCl buffer concentration for the dehalogenase activity was found to be 50 mM.

The apparent V_{\max} obtained for 1-chlorobutane conversion with resting *Xanthobacter autotrophicus* GJ10 cells was $0.35 \mu\text{mol min}^{-1} \text{g}^{-1}$ of cells and the apparent K_m was 2.8 mM of 1-chlorobutane. The V_{\max} and K_m for 1-chlorobutane hydrolysis by the free dehalogenase, as determined by Schindler et al. (1999), were $3.1 \mu\text{mol min}^{-1} \text{mg}^{-1}$ of protein and 4.1 mM of 1-chlorobutane, respectively. Thus, the affinity for 1-chlorobutane is weaker for free purified enzyme than with whole cells.

Rhodococcus erythropolis NCIMB 13064 possesses a haloalkane dehalogenase that forms part of the same family of the α/β hydrolases as that of the *Xanthobacter autotrophicus* GJ10 dehalogenase. Moreover, lyophilized cells of this strain have recently been studied in the gas phase for their ability to perform halogenated alkane transformation (Erable et al., 2004, 2005). These two strains are known to convert short haloalkanes such as 1-chlorobutane in the aqueous phase but *Rhodococcus erythropolis* cells

has a higher affinity for this substrate (0.4 mM) compared to 2.8 mM for *Xanthobacter autotrophicus* GJ10 and the apparent V_{\max} of 1-chlorobutane conversion is 7 times higher than that observed with *Xanthobacter autotrophicus* cells ($2.40 \mu\text{mol min}^{-1} \text{g}^{-1}$).

In the aqueous phase, there were some clear differences in terms of 1-chlorobutane dehalogenation between the two strains, *Xanthobacter autotrophicus* GJ10 and *Rhodococcus erythropolis* NCIMB 13064. The dehalogenase of *Rhodococcus erythropolis* NCIMB 13064 offers many advantages such as a higher affinity for 1-chlorobutane, a higher V_{\max} and greater temperature stability. Usually, the use of a catalyst directly in the gas phase provides greater temperature stability and a higher V_{\max} compared with the liquid phase. Thus, the question was: How might dehydrated *Xanthobacter autotrophicus* GJ10 behave in the gas phase?

Continuous 1-Chlorobutane Transformation by Lyophilized Cells of *Xanthobacter autotrophicus* GJ10 in a Solid-Gas Biofilter: Comparison With *Rhodococcus erythropolis* NCIMB 13064 Cells

In a recent article, the ability of dehydrated *Rhodococcus erythropolis* cells to transform 1-chlorobutane in a solid-gas biofilter was reported (Erable et al., 2004, 2005). We proposed to study and compare the same hydrolysis reaction of 1-chlorobutane in butan-1-ol and HCl with another dehalogenating strain, *Xanthobacter autotrophicus* GJ10.

In a first test, 200 mg of lyophilized *Xanthobacter autotrophicus* GJ10 cells were placed in the solid-gas biofilter at 40°C. The total flow passing into the biofilter was fixed at $500 \mu\text{mol min}^{-1}$. a_{clbut} and a_w were fixed at 0.15 and 0.8, respectively. Butan-1-ol synthesis was monitored by GC analysis.

Figure 2 clearly shows that *Xanthobacter autotrophicus* GJ10 cells can transform 1-chlorobutane to butan-1-ol in

Table I. Comparison of the optimal parameters for the dehalogenase activities of *Xanthobacter autotrophicus* GJ10 and *Rhodococcus erythropolis* NCIMB13064 resting cells in the aqueous phase.

	<i>Xanthobacter autotrophicus</i> GJ10 cells	<i>Rhodococcus erythropolis</i> NCIMB13064 cells
Temperature (°C)	30	45
pH	8.4	9.0
Tris/HCl buffer concentration (mM)	50	50–100
Apparent V_{\max} ($\mu\text{mol min}^{-1} \text{g}^{-1}$)	0.35	2.40
Apparent K_m (mM)	2.8	0.4

Note: *Xanthobacter autotrophicus* cells were grown for 48 h on a LB medium at 30°C in 1-L aerobic flask containing 200 mL of medium. *Rhodococcus erythropolis* cells were grown for 48 h on a mineral medium at 30°C in 1-L sealed flasks containing 200 mL of medium to which 100 μL (0.96 mmol) were added. The cells were then harvested, washed, and suspended in Tris HCl. Different tests were carried out with 50 mL of cellular suspension to which 100 μL of 1-chlorobutane was added. Butan-1-ol production was measured by GC analysis.

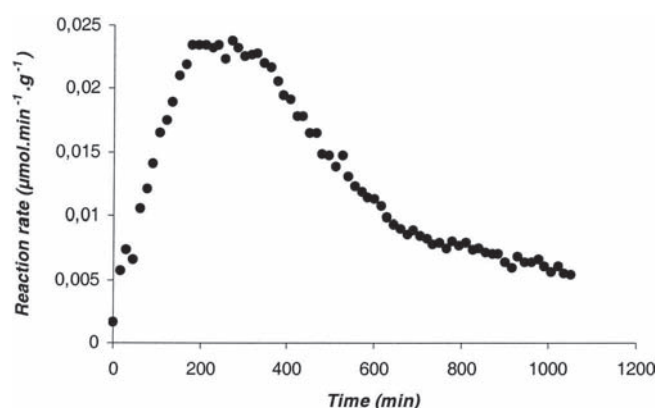


Figure 2. Reaction rate of 1-chlorobutane hydrolysis by dehydrated *Xanthobacter autotrophicus* GJ10 cells. The reaction was carried out at 40°C with 200 mg of dehydrated cells. The total flow passing into the biofilter was $500 \mu\text{mol min}^{-1}$; a_{clbut} and a_w were fixed at 0.15 and 0.8, respectively.

the gaseous phase, as was previously demonstrated with dehydrated *Rhodococcus erythropolis* cells. Moreover, only the dehalogenase seems to be active because the synthesized butan-1-ol wasn't degraded. Other secondary compounds were not detected in the gas phase leaving the reactor. This could be due either to the fact that only small amounts of catalyst were used and that we were not able to detect traces of secondary products, or to the fact that the enzymes involved in the butan-1-ol transformation require cofactors. Janssen et al. (1984, 1989) proposed that 1,2-dichloroethane is metabolized to 2-chloroethanol by an alcohol dehydrogenase using a PQQ cofactor and Maugard et al. (2001), found that natural cofactor regeneration was not possible in the gas phase with whole cells. Moreover, different tests of cell viability after cell dehydration showed that all the cells used in the gas phase tests were dead.

The initial rate of butan-1-ol formation corresponding to 1-chlorobutane dehalogenation increased to a maximal of $24.10^{-2} \mu\text{mol min}^{-1} \text{g}^{-1}$. The maximal initial rate obtained with these experimental conditions was nearly 100 times lower than that obtained with *Rhodococcus erythropolis* cells (Erable et al., 2004). This difference in behavior of the two dehydrated strains is in agreement with what has been described in the aqueous phase but the difference is even greater.

The conversion capacity of lyophilized *Xanthobacter autotrophicus* GJ10 cells was limited because of the loss of dehalogenase activity observed after 300 min of reaction (Fig. 2). This brutal fall could be due to (a) the effect of water on the catalyst acting as a denaturing agent with temperature; (b) 1-chlorobutane substrate inhibition by cell adsorption and accumulation or a denaturing effect; (c) butan-1-ol product inhibition; (d) HCl product inhibition by acidification of the dehalogenase catalytic site or by Cl^- binding to the catalytic site (Schindler et al., 1999). This loss of activity was already observed using *Rhodococcus erythropolis* NCIMB 13064 cells.

Inhibition by HCl Product During Reaction

In this study, the decrease in dehalogenase activity and the weak stability of the dehydrated cells observed in all tests could be attributed to a deactivation of haloalkane dehalogenase by substrates or products of the 1-chlorobutane hydrolysis reaction. Thermal inactivation can be excluded owing to the fact that the optimal temperature in the aqueous phase was 30°C for *Xanthobacter autotrophicus* GJ10 cells (Table I) and 37°C for the purified dehalogenase enzyme (Keuning et al., 1985). Moreover, greater thermal stability of the free enzyme has been demonstrated in gas phase systems (Cameron et al., 2002; Lamare et al., 2001).

To show which of the substrates (water and 1-chlorobutane) or products (butan-1-ol and HCl) were responsible for the dehalogenase inhibition, the different compounds were individually passed through a biofilter packed with cells for 400 minutes and a standard test (total flow of $500 \mu\text{mol}$

min^{-1} , a_w of 0.8 and a_{clbut} of 0.15) was then carried out. The results are presented on Figure 3.

When the catalyst was equilibrated with a water activity fixed at 0.8 for 400 min before being fed with 1-chlorobutane, a higher maximal reaction rate was noticed than when catalyst was directly fed with both water and 1-chlorobutane. These results confirm that catalyst was not denatured by the combined action of water and temperature.

No inhibition of dehalogenase activity was observed after 400 min of equilibration of the catalyst with 1-chlorobutane or butan-1-ol. These experiments thus clearly show that neither 1-chlorobutane nor butan-1-ol is involved in the inhibition of the catalyst.

On the contrary, an equilibration of the catalyst with HCl vapor during 200 minutes involves a complete inactivation of the dehalogenase activity.

These data suggest that the dehalogenase inhibition could be explained by HCl accumulation in the cells during the reaction. HCl is small hydrophilic molecule and probably diffuses slowly through the cell wall. Its accumulation could have several effects: (a) HCl accumulation in the microenvironment of the enzyme could cause an acidification of the active site and consequently the ionization state of the amino acids responsible for the activity could change. In a recent article, it was demonstrated that this inhibition could be blocked by the continuous addition of a volatile hydrophobic base (Erable et al., 2005); (b) HCl is a possible inhibitor of the *Xanthobacter autotrophicus* GJ10 dehalogenase. It has already been shown that Cl^- is an uncompetitive inhibitor of *Rhodococcus erythropolis* haloalkane dehalogenase (Schindler et al., 1999). The disruption of the bacterial cell wall also appeared to be a solution for avoiding HCl accumulation. Indeed, cell disruption could allow HCl diffusion and arrest the decrease in pH in the environment of the enzyme.

Cells Disruption Effect

To study the cell disruption effect, tests were carried out at 30°C with cells treated with lysozyme or by ultrasonic disruption. The biofilter was packed with 200 mg of treated and dehydrated cells, the total flow was fixed at $500 \mu\text{mol min}^{-1}$, a_w at 0.8, and a_{clbut} at 0.15.

A negative effect on dehalogenase activity was noticed (Fig. 4). Indeed, 1 minute of ultrasonic disruption treatment led to a decrease of 20% in the activity and with lysozyme treated cells the decrease was around 40%. The effect of *Xanthobacter autotrophicus* GJ10 cell disruption didn't correspond to the behavior of dehydrated *Rhodococcus erythropolis* cells treated with lysozyme as reported by Erable et al. (2004, 2005). The two strains are different in terms of the ultrastructure of their cell wall. *Xanthobacter autotrophicus* seems to have a Gram-negative type of cell wall while *Rhodococcus erythropolis* is known to be a Gram-positive bacterium. The disruption of the cell wall of *Xanthobacter autotrophicus* GJ10 could lead to an enzyme

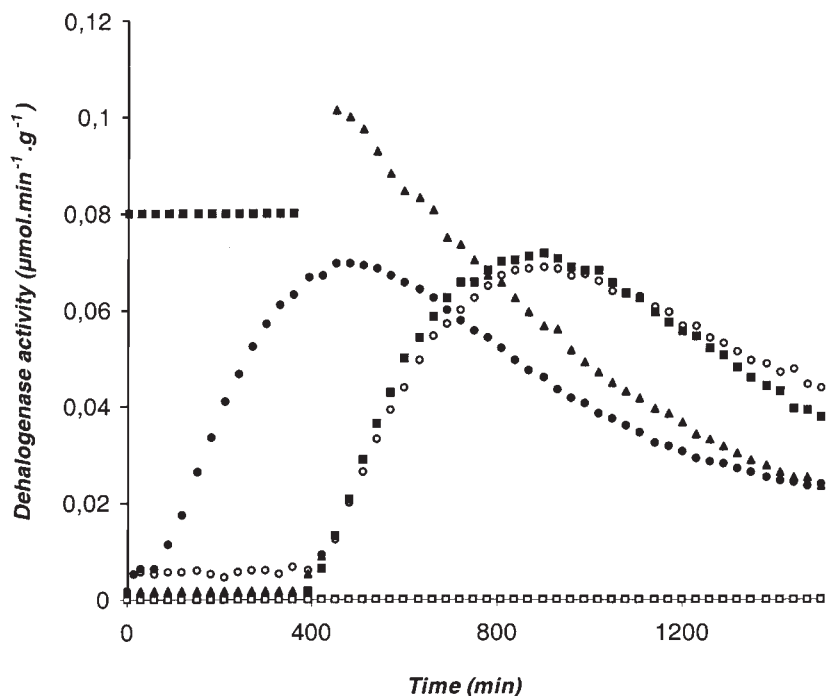


Figure 3. Effect of continuous treatment with substrates or products on the rate of 1-chlorobutane transformation catalyzed by dehydrated *Xanthobacter autotrophicus* GJ10. Reactions were carried out with 200 mg of lyophilized cells packed into the biofilter at 30°C with a total flow fixed at 500 $\mu\text{mol min}^{-1}$. (●) $a_w = 0.8$ and $a_{\text{clbut}} = 0.15$; (▲) $a_w = 0.8$ during 400 min and then $a_w = 0.8$ and $a_{\text{clbut}} = 0.15$; (○) $a_{\text{clbut}} = 0.15$ during 400 min and then $a_w = 0.8$ and $a_{\text{clbut}} = 0.15$; (■) butan-1-ol activity = 0.03 during 400 min and then $a_w = 0.8$ and $a_{\text{clbut}} = 0.15$; (□) HCl (30%) activity = 0.6 during 200 min and then $a_w = 0.8$ and $a_{\text{clbut}} = 0.15$.

destabilization and at the same time to a negative effect on dehalogenase activity. This hypothesis is supported by the data depicted in Figure 5, where the relative dehalogenase activity decreased with the time cells were exposed to ultrasonic disruption. It should be noted that

the same effect was obtained in the aqueous phase (data not shown).

Because disruption of cell wall induces a decrease of the dehalogenase activity, further tests in the gas phase were performed with whole dehydrated cells.

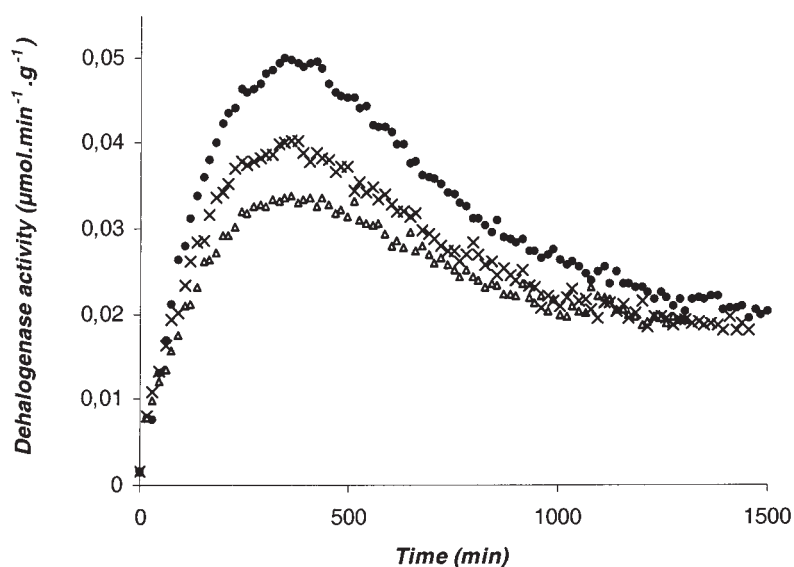


Figure 4. Rate of 1-chlorobutane transformation catalyzed by disrupted and dehydrated *Xanthobacter autotrophicus* GJ10 cells as a function of reaction time. Cells were disrupted by ultrasound treatment (×) or using lysozyme (△). The reaction was carried out with 200 mg of lyophilized cells packed into the biofilter at 30°C with a total flow fixed at 500 $\mu\text{mol min}^{-1}$. A_w and a_{clbut} were fixed at 0.8 and 0.15, respectively. Untreated cells were used as witness (●).

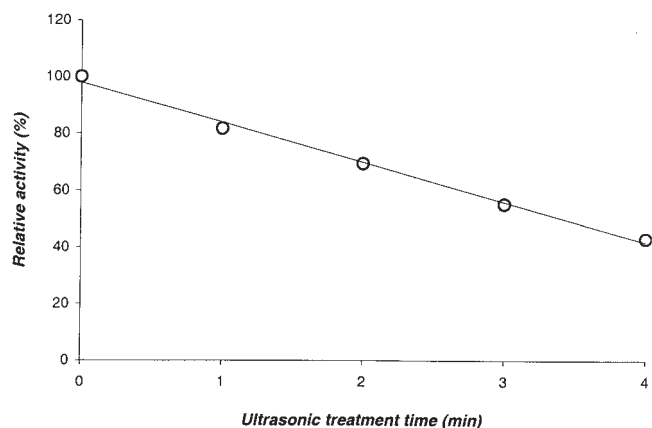


Figure 5. Effect of ultrasound treatment on relative dehalogenase activity of *Xanthobacter autotrophicus* GJ10. Cells were permeabilized by ultrasound treatment. The reaction was carried out with 200 mg of lyophilized cells packed into the biofilter at 30°C with a total flow fixed at 500 $\mu\text{mol min}^{-1}$. a_w and a_{clbut} were fixed at 0.8 and 0.15, respectively.

Water Activity (a_w) Effect on Dehalogenase Activity

The biofilter was packed with 200 mg of lyophilized cells. The total flow passing into the biofilter was 500 $\mu\text{mol min}^{-1}$ and the a_{clbut} was fixed at 0.15. All reactions were carried out at 30°C with different a_w conditions (0.5 to 0.85). The results are shown in Figure 6.

The initial rate of butan-1-ol synthesis increased under a_w conditions of 0.5 to 0.85. The water and substrate adsorption on dehydrated cells increased in a similar way. The relation between water sorption and dehalogenase activity could be explained by the fact that water is a substrate for the hydrolysis reaction and also probably that water adsorption supported molecular mobility and enzymatic flexibility (Graber et al., 2003). Over the range of tested a_w , optimal dehalogenase activity was obtained for an a_w of 0.85.

These results are in agreement with what has already been reported with *Rhodococcus erythropolis* cells (Erable et al., 2004) and with whole baker's yeast cells for alcohol dehydrogenase activity (Goubet et al., 2002; Maugard et al., 2001).

Temperature Effect

The effect of temperature on the dehalogenase activity of dehydrated cells in the gaseous phase was tested over a range of temperatures from 30°C to 60°C. The biofilter was packed with 200 mg of lyophilized *Xanthobacter autotrophicus* GJ10 cells and fed with 500 $\mu\text{mol min}^{-1}$ of gaseous phase; a_{clbut} and a_w were fixed at 0.15 and 0.8, respectively.

In the gaseous phase, the optimal temperature for *Xanthobacter autotrophicus* dehalogenase activity was 30°C and no activity was observed at temperatures higher than 50°C. The results obtained with dehydrated *Rhodococcus erythropolis* cells showed a constant increase of dehalogenase activity with temperatures from 30°C to

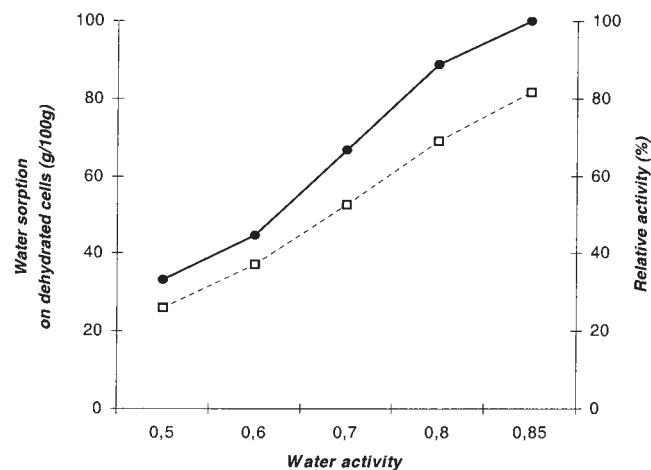


Figure 6. Effect of water activity on relative activity of *Xanthobacter autotrophicus* GJ10 cells (●) and on water cell adsorption (□). Reactions were carried out at 30°C with 200 mg of dehydrated cells. The total flow passing into the biofilter was 500 $\mu\text{mol min}^{-1}$; a_{clbut} and a_w were fixed at 0.15 and 0.8, respectively.

60°C (Erable et al., 2004). However, the results obtained with *Xanthobacter autotrophicus* GJ10 were different. In fact, *Xanthobacter autotrophicus* cells are more sensitive to thermal denaturation than *Rhodococcus erythropolis* cells even in the gas phase.

Effect of Buffer pH Before Dehydration

The optimal pH in the aqueous phase for cellular dehalogenase activity was found to be 8.4, whereas an optimal pH 8.2 was obtained with the purified enzyme (Keuning et al., 1985). In nonconventional media, enzyme activity is often dependent on the ionization state of the enzyme before dehydration (pH memory) (Zaks and Klivanov, 1985). Thus, *Xanthobacter autotrophicus* cells were lyophilized at different pH from 4.0 to 10.5 and tested in the solid-gas biofilter. The plot obtained for the dehalogenase activity of the dehydrated cells as a function of pH in the gaseous phase was similar to that obtained in the aqueous phase with an optimal pH of 8.4 (Fig. 7). Therefore, the pH memory of dehydrated cells exists in the gas phase too.

1-Chlorobutane Activity Effect

The effect of a_{clbut} on the dehalogenase of dehydrated *Xanthobacter autotrophicus* GJ10 cells was studied. The biofilter was packed with 200 mg of lyophilized cells and the total flow passing into the biofilter was fixed at 500 $\mu\text{mol min}^{-1}$ with an a_w of 0.8. Only a_{clbut} increased from 0.015 to 0.18 at 30°C. The results are reported in Figure 8.

The maximal reaction rate of butan-1-ol synthesis increased with a_{clbut} . The plot looked like a typical Michaelis-Menten enzyme-type and no inhibitory effect was observed

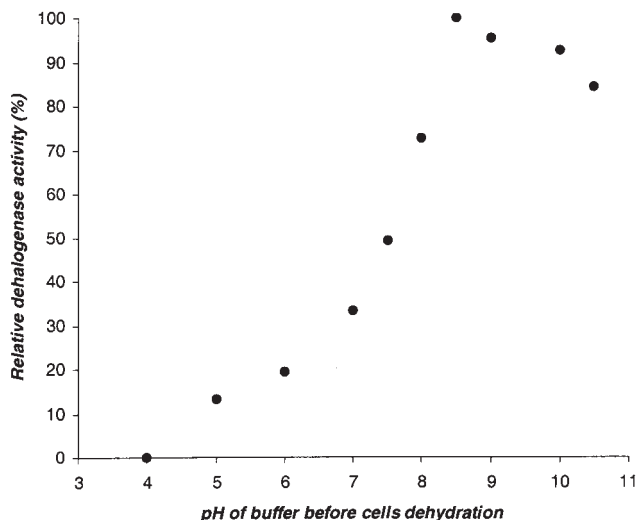


Figure 7. Effect of the pH of buffer before dehydration of cells on relative dehalogenase activity of *Xanthobacter autotrophicus* GJ10. The reaction was carried out with 200 mg of lyophilized cells packed into the biofilter at 30°C with a total flow fixed at 500 $\mu\text{mol min}^{-1}$. A_w and a_{clbut} were fixed at 0.8 and 0.15, respectively.

with high a_{clbut} . Reciprocal initial rates vs. reciprocal a_{clbut} were used to determine the apparent Michaelis-Menten constants V_{max} and K_m , taking into account the fact that the maximal a_{clbut} was 1. Thus, the apparent V_{max} of $8.10^{-2} \mu\text{mol min}^{-1} \text{g}^{-1}$ and K_m of 0.07 (1-chlorobutane thermodynamic activity) were determined at 30°C.

The apparent Michaelis-Menten constants V_{max} and K_m obtained with dehydrated *Rhodococcus erythropolis* cells

Table II. Effect of the total flow passing into the biofilter on the 1-chlorobutane transformation rate by dehydrated *Xanthobacter autotrophicus* GJ10 cells.

Total flow ($\mu\text{mol min}^{-1}$)	1-chlorobutane flow ($\mu\text{mol min}^{-1}$)	Residence time in the reactor (s)	1-chlorobutane transformation rate ($\text{nmol min}^{-1} \text{g}^{-1}$)
180	5.4	15.3	88
280	7.4	9.8	83
500	14.2	5.5	73
780	22.7	3.5	65

Note: Reactions were carried out at 30°C with 200 mg of dehydrated cells. The total flow passing into the biofilter was variable; a_{clbut} and a_w were fixed at 0.15 and 0.8, respectively.

were previously described by Erable et al. (2005). They reported an apparent V_{max} of $3.22 \mu\text{mol min}^{-1} \text{g}^{-1}$ and an apparent K_m of 0.011 (1-chlorobutane thermodynamic activity) at 40°C. Dehydrated *Rhodococcus erythropolis* cells had a higher affinity for the 1-chlorobutane substrate in the gaseous phase; this was also reported by the data obtained in the aqueous phase (Table I). Moreover, the rate of catalysis of 1-chlorobutane transformation was 40 times lower with dehydrated *Xanthobacter autotrophicus* cells, whereas this ratio was only 7 in the aqueous phase.

Effect of the Total Flow Passing Into the Biofilter

Using a total flow of 500 $\mu\text{mol min}^{-1}$, the *Xanthobacter autotrophicus* GJ10 dehalogenase activity was relatively weak. However, in a continuous process the reduction of

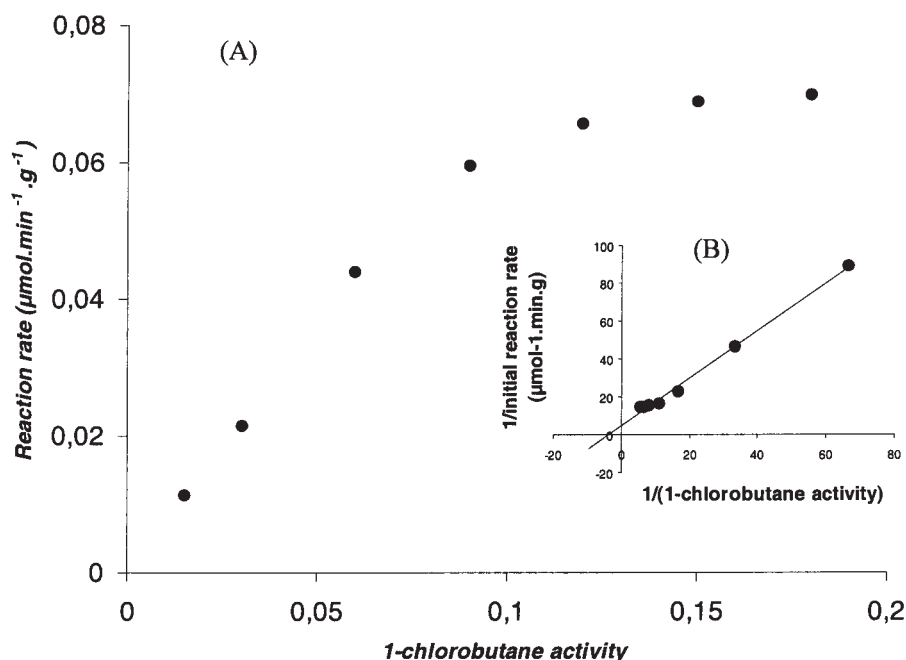


Figure 8. Reaction rate of the 1-chlorobutane transformation as a function of a_{clbut} (A) and reciprocal initial reaction rate of the hydrolysis of 1-chlorobutane vs. reciprocal a_{clbut} (B). Reactions were carried out at 30°C with 200 mg of dehydrated cells. The total flow passing into the biofilter was 500 $\mu\text{mol min}^{-1}$ and a_w was fixed at 0.8.

the total flow usually increases substrate conversion. It was decided to increase substrate residence time in the biofilter in an attempt to increase 1-chlorobutane degradation. Thus, the reaction rate was measured at different total flow while a_w and a_{clbut} were maintained constant (0.8 and 0.15, respectively).

Total flows tested for the 1-chlorobutane conversion varied from 180 to 780 $\mu\text{mol min}^{-1}$. The contact time between catalyst and substrate was 4.2-fold longer when the total flow was fixed at 180 $\mu\text{mol min}^{-1}$ (Table II). In fact, the residence time of the substrate was 15.3 s at 180 $\mu\text{mol min}^{-1}$ and only 3.5 s at 780 $\mu\text{mol min}^{-1}$. At the same time, the observed 1-chlorobutane transformation rate increase by 35% (65 $\text{nmol min}^{-1} \text{g}^{-1}$ to 88 $\text{nmol min}^{-1} \text{g}^{-1}$) when the total flow decreased from 780 to 180 $\mu\text{mol min}^{-1}$. These results clearly show that total flow passing into the gas phase biofilter do not influence too much the 1-chlorobutane conversion rate.

Effect of the Amount of Dehydrated Cells Packed Into the Biofilter

In Figure 2, the initial rate of butan-1-ol synthesis increased to a maximal value after 300 minutes of reaction and in a second phase butan-1-ol production decreased to almost zero. Using these experimental conditions (200 mg of dehydrated *Xanthobacter autotrophicus* GJ10 cells, total flow of 500 $\mu\text{mol min}^{-1}$, a_w of 0.8 and a_{clbut} of 0.15 at 30°C), 200 mg of catalyst cannot last more than 1500 hours.

Consequently, the effect of dehydrated cells packed into the biofilter on 1-chlorobutane transformation capacity was studied. The experimental conditions were fixed at 500 $\mu\text{mol min}^{-1}$ at 30°C with an a_w and a_{clbut} of 0.8 and 0.15, respectively. Only the quantity of cells packed into

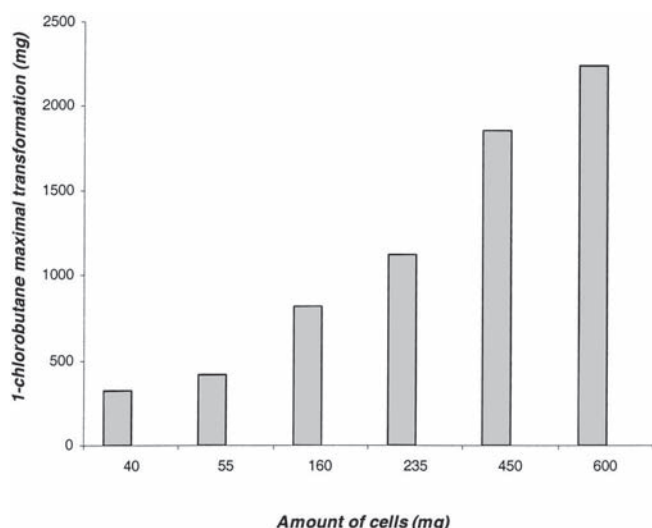


Figure 9. Maximal 1-chlorobutane transformation capacity of dehydrated *Xanthobacter autotrophicus* GJ10 cells as a function of the quantity of cells. The total flow passing into the biofilter was 500 $\mu\text{mol min}^{-1}$; a_{clbut} and a_w were fixed at 0.15 and 0.8, respectively.

the biofilter varied from 40 to 600 mg. The results show that the 1-chlorobutane transformation capacity of dehydrated *Xanthobacter autotrophicus* GJ10 cells is proportional to the amount of catalyst packed into the solid-gas biofilter (Fig. 9). We have estimated that 1 g of lyophilized cells can transform 1.4 g of 1-chlorobutane in 24 hours.

CONCLUSION

The ability of dehydrated *Xanthobacter autotrophicus* GJ10 cells to transform 1-chlorobutane in a solid-gas biofilter was initially highlighted. The behavior of this strain in the gas phase was different to that previously observed with *Rhodococcus erythropolis* NCIMB 13064. The low stability of continuous 1-chlorobutane dehalogenation was clearly due to the inhibition by HCl produced during the reaction and cells disruption did not prevent the accumulation of this product. The study of several important parameters in solid-gas biocatalysis (temperature, water thermodynamic activity, substrates thermodynamic activity, pH memory) made it possible to increase maximal the dehalogenase activity of whole cells.

Finally, while modulating the balance between the amount of cells packed into the biofilter and the total flow, it was estimated that 1 g of dehydrated *Xanthobacter autotrophicus* GJ10 cells could dehalogenate 1.4 g of 1-chlorobutane per day.

Our research is now concentrated on the problem of the stability of cell dehalogenase activity. A special effort is being undertaken to understand and to avoid the HCl accumulation in the cell.

We thank D.B. Janssen (Department of Biochemistry, Groningen Biotechnology Center, University of Groningen) for providing the *Xanthobacter autotrophicus* GJ10 strain.

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