## ADSORPTION OF PHENOL FROM ACCEOUS SOLUTIONS USING INCIDERATED STALLAR SOLUTIONS

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#### ADSORPTION OF PHENOL FROM AQUEOUS SOLUTIONS USING INCINERATED SEWAGE SLUDGE

By

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Thesis submitted to the School of Graduate Studies, Universiti Putra Malaysia, in Fulfillment of the Requirements for the Degree of Masters of Science

November 2004

 $\mathcal{T}_{0}$  mum and dad,

# This is for you...

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#### ABSTRACT

A study had been carried out to determine the potential use of sewage sludge ash (SSA) as an adsorbent in removing phenol from aqueous solution. Parameters which contributed to affect phenol removal were initial phenol concentration, contact time, adsorbent dosage, pH and particle size of adsorbent. Results showed that the adsorption capacities of adsorbent (K<sub>f</sub>) for phenol decreased from 14.89 mg/g to 0.68 mg/g as initial phenol concentration increased from 0.1 mg/l to 5.0 mg/l. Results revealed that solution with higher initial phenol concentration required longer time to reach equilibrium state. Adsorption capacity of adsorbent (Kf) decreased from 14.89 mg/g to 0.66 mg/g as contact time increased from 240 minutes to 1200 minutes. Furthermore, pH was found to affect the adsorption capacity where as pH decreased from original (9 - 12) to neutral (7 - 8), adsorption capacity of adsorbent increased from 0.68 mg/g to 3.0 mg/g. Moreover, it was shown that as particle size of adsorbent decreased from 150 - 212 µm to 63 - 149 µm, adsorption capacity of adsorbent (K<sub>f</sub>) was decreased from 2.06 mg/g to 0.68 mg/g. Adsorption isotherm analysis showed that the experimental data fit Freundlich model in most conditions.

#### ABSTRAK

Kajian telah dilakukan untuk mengetahui potensi abu enapcemar kumbahan dalam penyingkiran "phenol" daripada larutan berair. Parameter-parameter yang mempengaruhi penyingkiran 'phenol" terdiri daripada kepekatan awal "phenol", masa tindakbalas, dos penyerap, nilai pH dan saiz butiran penyerap. Keputusan menunjukkan bahawa kapasiti penyerapan abu enapcemar (Kf) bagi "phenol" menurun daripada 14.89 mg/g kepada 0.68 mg/g apabila kepekatan awal "phenol" meningkat daripada 0.1 mg/l kepada 5.0 mg/l. Keputusan mendedahkan bahawa larutan dengan kepekatan awal "phenol" yang lebih tinggi memerlukan lebih lama masa untuk mencapai keadaan keseimbangan. Kapasiti penyerapan bagi abu enapcemar (K<sub>f</sub>) menurun daripada 14.89 mg/g kepada 0.66 mg/g apabila masa tindakbalas meningkat daripada 240 minit kepada 1200 minit. Selain itu, nilai pH didapati mempengaruhi kapasiti penyerapan iaitu apabila nilai pH menurun daripada keadaan semulajadi (9 - 12) kepada neutral (7 - 8), kapasiti penyerapan abu enapcemar meningkat daripada 0.68 mg/g kepada 3.0 mg/g. Selain daripada itu juga, telah ditunjukkan bahawa apabila taburan saiz butiran abu enapcemar menurun daripada 150 - 212 µm kepada 63 - 149 µm, kapasiti penyerapan abu enapcemar (K<sub>f</sub>) menurun daripada 2.06 mg/g kepada 0.68 mg/g. Analisis penyerapan isoterma menunjukkan bahawa data ujikaji sesuai dengan model Freundlich dalam kebanyakan keadaan.

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I sincerely hope that this study will be a contribution toward the goal of better engineering in the field of water quality. I constantly remind myself of the following quote from Baba Diodum; "In the end we will conserve only what we love, we will love only what we understand and we will understand only what we are taught".

Should there be any omissions, I would like to offer my apologies in advance. There is little, apart from mistakes, for which I can claim credit. My contribution, if any, is in correlation and interpretation of the available information. Even on this there are bound to be differing views, because the entire scientific truth on the subject has not yet been revealed, and interpretations at variance do not imply criticism or disrespect.

Finally, I would like to thank all people, whose have been helping me in this study and especially to my parent for giving me support in my life. I certify that an Examination Committee met me on 3 November 2004 to conduct the final examination of Wan Afnizan Bin Wan Mohamed on his Masters of Science thesis entitled "Adsorption of Phenol from Aqueous Solution Using Incinerated Sewage Sludge" in accordance with Universiti Pertanian Malaysia (Higher Degree) Act 1980 and Universiti Pertanian Malaysia (Higher Degree) Regulations 1981. The Committee recommends that the candidate be awarded the relevant degree. Members of the Examination Committee are as follows:

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#### DECLARATION

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I hereby declare that the thesis is based on my original work except for quotations and citations which have been duly acknowledged. I also declare that it has not been previously or concurrently submitted for any other degree at UPM or other institutions.

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WAN AFNIZAN BIN WAN MOHAMED

Date: 9 November 2004

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- Figure B.6 Langmuir adsorption isotherm of sewage sludge for phenol 131 at Adsorbent dosage = 7.0 g; Co = 5.0 mg/l; T = Room (28 ± 2 °C); pH = Original (9 - 12); Particle size = 63 - 149 μm.
- Figure B.7 Freundlich adsorption isotherm of sewage sludge for 132 phenol at Adsorbent dosage = 7.0 g; Co = 0.1 mg/l; T = Room (28 ± 2 °C); pH = Original (9 - 12); Particle size = 63 - 149 µm.

- Figure B.8 Freundlich adsorption isotherm of sewage sludge for 132 phenol at Adsorbent dosage = 7.0 g; Co = 5.0 mg/l; T = Room (28 ± 2 °C); pH = Original (9 - 12); Particle size = 63 - 149 μm.
- Figure B.9 Langmuir adsorption isotherm of sewage sludge for phenol 133 at Contact time = 240 minutes (4 hours) for 0.1 mg/l;
  T = Room (28 ± 2 °C); pH = Original (9 12), Particle size = 63 149 μm.
- Figure B.10 Langmuir adsorption isotherm of sewage sludge for phenol 133 at Contact time = 1200 minutes (20 hours) for 5.0 mg/l;  $T = Room (28 \pm 2 \text{ °C}); pH = Original (9 - 12), Particle size$ = 63 - 149 µm.
- Figure B.11 Freundlich adsorption isotherm of sewage sludge for 134 phenol at Contact time = 240 minutes (4 hours) for 0.1 mg/l; T = Room (28 ± 2 °C); pH = Original (9 12), Particle size = 63 149 μm.
- Figure B.12 Freundlich adsorption isotherm of sewage sludge for 134 phenol at Contact time = 1200 minutes (20 hours) for 5.0 mg/l; T = Room (28 ± 2 °C); pH = Original (9 12), Particle size = 63 149 μm.
- Figure B.13 Langmuir adsorption isotherm of sewage sludge for phenol 135 at pH 9 - 12 (original) and pH 7 - 8 (normal); T = Room (28 ± 2 °C).
- Figure B.14 Figure 4.36: Freundlich adsorption isotherm of sewage 135 sludge for phenol at pH 9 12 (original) and pH 7 8 (normal); T = Room (28 ± 2 °C).
- Figure B.15 Langmuir adsorption isotherm of sewage sludge for phenol 136 at 63 - 149  $\mu$ m and 150 - 212  $\mu$ m; T = Room (28 ± 2 °C); pH = Original (9 - 12).
- Figure B.16 Freundlich adsorption isotherm of sewage sludge for 136 phenol at 63 149  $\mu$ m and 150 212  $\mu$ m; T = Room (28 ± 2 °C); pH = Original (9 12).
- Figure C.1 Electrical oven, Memmert, model ULM400 Schwabach, 138 Germany.
- Figure C.2 Muffle furnace, CWF 11/5, England. 138
- Figure C.3 (a) British Standard Sieve (BS410/1986) (b) Sewage 139 sludge ash was sieved on test sieve shaker for a period of 15 minutes.

| Figure C.4 | Adsorbent was kept inside desiccator.                                 | 139         |
|------------|---|-------------|
| Figure C.5 | Analytical balance, Precisa XT220A, Swiss.                            | 140         |
| Figure C.6 | Flask shaker, SF1, UK.  | 140         |
| Figure C.7 | pH for mixture was measured using pH-meter, Cyberscan 500, Singapore. | 14 <b>1</b> |
| Figure C.8 | UV spectrophotometer, Genesys <sup>™</sup> 2PC, model 336003, USA.    | 141         |

#### LIST OF SYMBOLS

| Co             | Initial phenol concentration (mg/l).  |
|----------------|---|
| Ce             | Phenol concentration in solution at equilibrium (mg/l).   |
| K <sub>d</sub> | The equilibrium constant.   |
| K <sub>f</sub> | Adsorption capacity (mg/g).   |
| 1/n            | Adsorption intensity.   |
| Mı             | Phenol concentration of stock solution (mg/l).  |
| M <sub>2</sub> | Phenol concentration to be prepared (mg/l).   |
| q <sub>e</sub> | The amount of phenol adsorbed at equilibrium (mg/g).  |
| q <sub>m</sub> | The maximum adsorption capacity of adsorbent (mg/g).  |
| Vı             | Volume of solution needed to be taken from stock solution (ml).                                     |
| V <sub>2</sub> | Volume of distilled water to be added into diluted volumetric flask until it reached the mark (ml). |
| ф              | Diameter.   |