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- State of the art of the environmental behaviour and removal techniques of the
 endocrine disruptor 3,4-dichloroaniline
- 3

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5 Abstract

6 In recent years, the presence of Endocrine Disrupting Chemicals (EDCs) in wastewater 7 discharges from agricultural and industrial sources, ^[1] fresh- and estuarine-waters, as well as 8 soils, has been reported in the literature. ^[2] Studies of adverse changes in wildlife, linked to 9 environmental exposure to these substances, and the suggestion that humans could also be at 10 similar risk of adverse health effects, ^[3-5] have raised concern for urgent action to understand 11 and reduce such risks. 3,4-dichloroaniline (3,4-DCA) has been recognized as an EDC, with 12 regards to endocrine disruption data for both wildlife populations and human health. ^[5]

3,4-DCA is present in the environment as a product of the biodegradation of phenylurea and phenylcarbamate pesticides; ^[6, 7] furthermore, it can be introduced from industrial and municipal wastewater that is insufficiently purified, or via accidental spills. ^[8-10] Increasing concentrations of 3,4-DCA in soil and water are the result of its high persistence and accumulation, as well as its low biodegradability. ^[11, 12] Hence, remediation techniques require in-depth study, especially when considering the low removal achieved by traditional activated sludge treatments, and the generation of carcinogenic trihalomethanes as a consequence of the chlorine oxidation methods

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frequently used in drinking water plants. ^[13] Fe⁰/H₂O₂ systems, photodegradation using doped
TiO₂, and the use of dielectric barrier discharge reactors, seem to be the most promising
techniques for the removal of 3,4-DCA from water.

27 Keywords: 3,4-DCA; water; environment; pollution; adsorption; electrochemistry

28 Introduction

Global annual production of 3,4-dichloroaniline (3,4-DCA) was ~42-47 kt prior to 1986 ^[14] and, 29 30 although recent years have seen a decrease in scale, EU production was still around 13.5-15.5 kt annum⁻¹ in the period 1996-1998. ^[15] 3,4-DCA, a derivative of aniline, is an 31 32 intermediate in the chemical synthesis of 3,4-dichlorophenylisocyanate, to make phytosanitary products, such as propanil, linuron, diuron, and neburon, ^[15-17] used to treat crops including rice, 33 potatoes, beans and tobacco.^[18] It is also employed in the synthesis of azo dyes for polyester 34 fabrics ^[17] and pharmaceuticals. ^[5] Although there is no exposure risk for vulnerable groups 35 36 from direct use of 3.4-DCA, indirect contact is expected via food, primarily fruit and vegetables, ^[5] as a result of the hydrolysis and biological degradation of phenylurea, phenylcarbamates and 37 acylchloroanilide pesticides present in soils, ^[19-27] by field waters and plant enzymes. ^[28] 38 Furthermore, industrial wastewater ^[11] may contain 3,4-DCA, mainly from microbial conversion 39 of 3,4-dichloro-1- nitrobenzol within water treatment plants. [5, 28] 40

In this manuscript, we summarize the current knowledge concerning the introduction,
movement, and fate of 3,4-DCA in the environment. We discuss the state-of-the-art remediation
technologies currently in use, as well as those under development, with reference to their
effectiveness for pollutant removal from soil and water systems.

45 Toxicity

46 In humans, EDCs are known to affect male and female reproductive organs, thyroid metabolism,
47 ^[29-31] breast development, cardiovascular and neuro-endocrinology, ^[32] causing obesity and

some cancers, including prostate cancer. ^[33] Little is known about the mechanisms of action of these substances, nor their physical and chemical diversity, hence, additional research into EDCs is required, especially on the cumulative impact of EDC mixtures, which may be additive or synergistic, ^[32, 34] even when individual chemicals are present below the threshold of detectable effects. ^[35] Consequently, the current lack of knowledge regarding exposure scenarios hinders the assessment of human health risk and impact. ^[36]

54 Chloroanilines can negatively affect soil microflora, and the presence of phenylamide herbicide degradation products has been shown to inhibit Nitrosomonas, hence, soil nitrification. ^[37] 3,4-55 DCA primarily acts by polar narcosis on aquatic organisms; ^[38, 39] fish and crustaceans are 56 extremely sensitive with respect to water column exposure, while annelids are greatly affected 57 by exposure to the sediment.^[17] Tests have demonstrated the relatively low, acute toxicity of 58 59 3,4-DCA on marine and fresh water animals, as well as unicellular algae, but there are significant chronic effects ^[40, 41] with consequences for marine life reproduction, ^[4] including 60 changes in secondary sex characteristics; ^[42] while rats have shown significant hormonal effects. 61 62 ^[3] As a consequence of these impacts, Predicted No-Effect Concentrations (PNECs) have been proposed, which are $0.2 \ \mu g \ L^{-1}$ for freshwater and seawater bodies, and $0.1 \ mg \ kg^{-1}$ dry weight 63 (0.04 mg kg⁻¹ wet weight) by mass ^[17] for sediments. 64

65 Environmental behaviour and fate

66 Chloroanilines are known to diffuse easily within the natural environment, ^[1, 14] and are very 67 difficult to remediate, hence, their concentration in soils and waters is increasing due to their 68 high persistence, accumulation, ^[11, 12] low biodegradation ^[43] and low leaching potentials. ^[44] 69 By contrast, 3,4-DCA is barely measured in water bodies, ^[5] and it occurs in higher aqueous 70 concentrations than the parent herbicide diuron. ^[45] It has been detected in European surface 71 waters, ^[16, 46] and its migration is determined by transport and retention mechanisms. ^[47] Hydrolysis of 3,4-DCA is not considered a mitigating mechanism due to aromatic stabilisation
effects, ^[48] and, as a result of its relatively low Henry's constant (K_H), it is not expected to
volatilise from water columns. ^[17, 48] Rather, as the physical data presented in Table 1 show, 3,4DCA losses from natural waters occur via photochemical degradation, or adsorption on sediment
and dissolved humic materials. ^[49] To this end, photo-transformation is the major degradation
pathway of 3,4-DCA in environmental waters, ^[16] maximised at 300 nm, well within the solar
spectrum observed at sea level. ^[4]

79 Table 1. Properties of 3,4-dichloroaniline

Property	Value	Ref.	
Molecular formula	C ₆ H ₅ Cl ₂ N	-	
Molecular structure		[15]	
Appearance	Solid at 293 K	[15]	
Molecular weight	162 g mol ⁻¹	[15]	
Molecular size	0.35 nm ²	[50]	
Henry's constant	0.05 Pa m ³ mol ⁻¹	[15]	
Solubility in water	580 mg L ⁻¹ at 293 K	[15]	
Octanol-water partition coefficient (log Kow)	2.7 (shaken flask method)	[5, 16]	
Estimated surface water half life	18 days	[15]	
Measured rate of loss from outdoor water systems	0.11 - 0.17 day ⁻¹	[4]	
	0.06 - 0.14 day ⁻¹	[49]	
Estimated atmospheric half life	9 hours	[15]	
Estimated half-life in soil and sediment	470 - 1500 days	[51]	

It is known that soil mobility and bioavailability of pollutants, and their degradation products, 80 depend on a combination of adsorption and desorption by soil components.^[47] The binding 81 82 effect of soil generally increases with time, leading to a decrease in pollutant bioavailability and toxicity, due to meteoric leaching. ^[52] Hence, the majority of 3,4-DCA released into the 83 environment accumulates, over time, on the organic fraction of sediments and soils.^[15] On the 84 other hand, sorption on dissolved macromolecules and colloidal particles promotes transport in 85 86 subsurface environments. ^[53] When chloroanilines are released into the soil with herbicides, only a small portion of the former is mineralized, consequently, many chloroanilines persist for 87 years, ^[54] often immobilized by interaction with humic substances, as mentioned above. ^{[9, 20, 55,} 88 ^{56]} Therefore, it is only a small fraction of liberated chloroanilines that undergo dimerization or 89 polymerization, by microbial oxidases and peroxidases, forming stable azo compounds. ^[47, 57] 90 Surface adsorption, due to van der Waals forces or electrostatic interactions, is often the initial 91 92 phase of pollutant binding by soil, while stronger bonds may occur over time.^[1] Consequently, 93 fulvic and humic acids play a significant role in the binding of xenobiotics, such as 94 chloroanilines, from aqueous media, via functional substituents, including hydroxyl, carboxylic acid, ketone, amino acid, saccharide and aminosaccharide groups.^[58, 59] Aniline sorption to soil 95 96 involves stronger interactions, starting with hydrophobic partitioning and cation exchange, 97 before covalent bonding, due to the contribution of limited energy or availability of sorption sites, occurs. 3,4-DCA adsorbs onto sediment ^[49] and soil particles, building stable, most 98 probably, covalent bonds with organic substances. ^[16, 17] Such initial reversible equilibrium, 99 followed by a slower irreversible mechanism, is well described by a biphasic kinetic model. ^{[60,} 00 101 61] Similar information on the sorption mechanisms of 3,4-DCA is fundamental to the 102 development of remediation strategies. In laboratory experiments, more than 70% of radio 103 labelled 3,4-DCA was found, as stated above, to bind to sediment and suspended matter in a water column; ^[62] ~80% of radioactivity was removed from the water column within 8 days, and 104

~99% after 90 days, ^[63] suggesting an initially quick process, which then plateaus and requires 105 106 significant time to reach its final equilibrium. As a consequence of the proposed interaction 107 between 3,4-DCA and organic materials, the interactions between dissolved organic matter from 108 soil, organic contaminants, and other soil components strongly affect the fate of 3,4-DCA in soil and water systems. ^[64-67] As a result, increasing soil organic carbon content, via organic matter 109 110 amendments to a soil sample, which may also introduce dissolved organic matter, can potentially enhance sorption, and decrease leaching, of pollutants, ^[68, 69] including 3-4-DCA; ^[49] 111 112 notably, similar results have been observed for organic matter amendment of inorganic soils.^{[8,} 47] 113

A study into the interaction of various humic fractions and the herbicide diuron ^[70] showed that the main degradation product, 3,4-DCA, was irreversibly bound on humic acids within days of formation. As a result, the risk of pollutant leaching is expected to be low for soils with high humic or fulvic acid contents. The irreversible sorption observed in these systems was described using a Freundlich isotherm model:

$$C_{s} = K_{f}C_{e}^{n}$$
(1)

119 where C_s is the concentration of 3,4-DCA sorbed ($\mu g g^{-1}$), C_e is the equilibrium solution 120 concentration of 3,4-DCA ($\mu g m L^{-1}$) and K_f (mL g⁻¹) expresses the soil sorption capacity. The 121 exponent *n* is related to the degree of isotherm nonlinearity, and provides an indication of the 122 favourability of the sorption process. ^[71]

The results of Freundlich analysis indicated that humic fractions have a sorptive capacity ten times that of their fulvic counterparts, due to preferential reaction of the amino groups of 3,4-DCA with the carboxyl and carbonyl groups of soil humic fractions, leading to the formation of soil bound residues, ^[72, 73] as confirmed by high adsorption and small desorption rates constants. 128 which a fraction of the pollutant physically binds to organic and inorganic soil components, while another fraction strongly adsorbs on the organic component. ^[43] Similarly, soil samples, 129 130 agitated in aqueous solutions of 3,4-DCA, have shown significant pollutant removal within 31 15 minutes of exposure and full equilibration, demonstrating up to 70% removal, after 50 hours. 32 The authors of this previous study reported the presence of two associated processes, firstly a 33 physical reaction, seemingly followed by chemical bond formation between 3,4-DCA and 34 organic matter within the soil, giving biphasic kinetics with rate constants of 4.9 hour⁻¹, for physical accumulation, and 0.03 hour⁻¹, for chemisorption. ^[49] Similar kinetic performance has 35 been observed for different agricultural soils and 3-4-DCA, ^[43] with sorption equilibrium 36 137 reached within 48 hours regardless of initial pollutant concentration, up to 16.2 µg mL⁻¹. Again, 38 the data was satisfactorily described by the Freundlich equation, and the amount sorbed was highest for the sandy clay loam soil used in the study ($K_f = 52 \text{ mL g}^{-1}$), as a consequence of its 139 140 higher organic matter content compared to the other soils studied, and the fact that it creates a 141 slightly acidic pH within the sorption system. By contrast the lowest sorption capacities were 142 obtained for calcareous silty clay soil and sand.

143 As initial adsorbate concentration increases, the availability of adsorption sites decreases, as 144 confirmed by n values lower than 1; such sorption behaviour being expressed by L-type 145 isotherms. ^[74] K_{oc} values, representing the sorption constant per gram of organic carbon in the 146 soil sample studied, show significant probability for 3,4-DCA contamination of ground-water for soils with lower sorption potentials.^[44] This is due to the strong relationship exhibited 147 148 between the sorption capacity and organic matter content of soil samples, and the fact there is 49 less impact with respect to clay content or a material's cation exchange capacity. It is also 50 noteworthy that consideration of soil organic content alone is insufficient to determine expected 51 sorption behaviour; for example, a lower level of diuron sorption is expected on clay-rich soils, 152 most likely as a result of a reduction in available binding sites in humic substances, due to the

positive interactions between humic materials and clay. ^[70] Soil pH may be another factor that 153 154 impacts on sorption of 3,4-DCA, as demonstrated by a reduction in K_f values, by ~50%, after liming of aqueous solutions.^[43] Such a trend probably results from the presence of aniline 155 functionalities within the soils tested, which are normally protonated species under the usually 56 acidic conditions found in such media, becoming neutral species as pH increases. [61, 75, 76] 57 Samples of calcareous soil mixed with aqueous 3,4-DCA, and allowed to equilibrate fully ^[47] 58 showed high K_f values, which indicates that adsorption is concentration dependent, ^[77] thereby 59 validating the assumption that adsorption on such solid media occurs primarily via hydrophobic 60 interactions due to the neutralisation of aniline functional groups at high soil pH. [73, 78] 161 162 Additional confirmation is provided by consideration of the physical properties of 3,4-DCA; Kow is known to be high, $^{[9, 79]}$ its solubility on water is low, combined with a K_{oc} of 338.6 L kg⁻¹ 163 $(K_{oc} = K_d/[organic content] \times 100$, where K_d is a measure of the distribution ratio of organic 164 65 molecules between the sorbed phase and solution), this all suggests that 3,4-DCA has a low potential for groundwater contamination in calcareous soils with high organic matter content. 166

167 Dissolved organic matter has been proven to compete with organic pollutants for the sorption sites available on soil surfaces, ^[80, 81] as well as in the building of stable bonds between pollutant 168 species and soil; ^[82] this competition enhances the apparent solubility of organic pollutants, 169 thereby reducing sorption and increasing their mobility. ^[67, 83] In contrast, dissolved organic 170 171 materials applied in soils may actually be adsorbed to soil surfaces, increasing sorption of hydrophobic organic compounds, ^[84] especially when tannic acid is added. ^[8] Inclusion of 172 173 dissolved organic carbon extracts, derived from both a commercial peat and high-purity tannic acid, to a soil sample showed significant impact on the sorption of 3,4-DCA. ^[47] The K_{d,DOC} 174 coefficient, defined as X_{doc}/C_{doc} (where X_{doc} is mg L⁻¹ of dissolved organic carbon and C_{doc} is 175 the corresponding equilibrium concentration), is consistently higher than the K_d values obtained 176 177 for undoctored soil, thereby confirming the influence of dissolved organic carbon on 3,4-DCA

sorption. Further confirmation is provided by an increase in 3,4-DCA sorption in the presence
of an environmental matrix, including inorganic ions and organic matter. ^[85] Sorption on
sedimentary material, hosted in a sediment extract media, was higher than for pure or run-off
waters, likely facilitated by previously sorbed dissolved organic content on the sediment surface,
present as a result of physical interactions between the two species. ^[73]

83 Remediation technologies

Remediation technologies developed for the destruction of chloroanilines present in wastewaters can be classified as physicochemical, chemical (oxidation) or biological, and are discussed in detail below. In essence, physicochemical methods utilise either adsorption, ion exchange, electrolysis or photodegradation, chemical processes require a chemical reaction with a selected additive, while biological degradation involves the action of aerobic or anaerobic microorganisms.

190 Bioremediation

191 Bacteria

92 3,4-DCA is not readily biodegradable; ^[17] the process being particularly slow in aqueous media. 93 Incubation of pond water, and pond water containing sewage sludge inoculum, in a darkened 94 environment showed that, after a period of 2 weeks, 97% of 3,4-DCA was recovered from the former sample and marginally less (94%) was recovered for the sample containing sewage, 195 indicating little biodegradation of the pollutant. ^[86] Similarly, no biodegradation was reported, 96 over the same time period, for an OECD 301 C test [87] with activated sludge, [88] nor after 97 4 weeks for an OECD 301 D test on activated sludge, and less than 5% degradation was 98 observed after 29 days for an OECD 303 A test, ^[87] again using activated sludge. ^[17] 199 Researchers also observed no discernible removal of 3,4-DCA from contaminated North Sea 200

water samples, ^[89] while only primary degradation occurred after one month using river water as
an inoculum. ^[90]

203 Usually, xenobiotics need to be in an aqueous phase in order to allow bacterial degradation to 204 occur. The 'bioaccessible fraction' of a pollutant is given by the sum of its concentration in pure 205 water, known as the 'bioavailable fraction', plus the 'potentially available fraction', which is 206 the material reversibly sorbed on any material surfaces. The addition of fulvic and humic acids 207 to inoculated soils was seen to decrease the rate of diuron degradation, reducing bioavailability 208 but not bioaccessibility, hence, lengthening the treatment time required; so it was only after 32 days that all diuron was degraded to 3,4-DCA.^[70] Hence, bioaccessibility is a better 209 210 indicator than bioavailability of the long-term influence of humic substances on diuron 211 degradation. The mineralisation rate of 3.4-DCA in soils is low, and it decreases as pollutant concentration increases; ^[15] only 3.9-11.9% mineralisation of 1 mg kg⁻¹ radio labelled 3,4- DCA 212 213 was recorded after 16 weeks within various soil types. ^[51] Degradation of 50% of 3,4-DCA was 214 observed in soil slurries with indigenous soil populations, and this was only marginally influenced by the addition of buffer, mineral salts and acetate. ^[91] In non-acclimated sediments, 215 216 dechlorination of applied 3,4-DCA started after 20 days, with anaerobic conversion to 3-217 chloroaniline (44%) and 4-chloroaniline (33%) within two months; these metabolites were not 218 further degraded. ^[92]

The microbial strains *Pseudomonas* acidovorans ^[93] and *Pseudomonas* diminuta ^[94] are able to use chlorinated anilines as a sole source of carbon and energy ; the latter also being capable of growing on 3,4-DCA. ^[95] Addition of *Pseudomonas* acidovorans to 3,4-DCA enriched soil slurries enhanced pollutant mineralization, leading to complete elimination of chloride after 10 days. ^[91] Up to 250 mg L⁻¹ of the pollutant and its intermediates were anaerobically degraded, in under 7 days, by a strain of *Pseudomonas* fluorescens. Without added glucose and nitrogen sources, degradation was slower, with 40% of toxicant removal in the first 15 days, at an initial concentration of 75 mg L⁻¹. ^[96] *Pseudomonas* diminuta was proven to dechlorinate up to 50 μ g mL⁻¹ of 3,4-DCA within its growth process, increasing the ratio of degradation in water samples from natural water reservoirs ^[97] and in fish ponds, where significant degradation of reversibly sorbed pollutant was observed within the first 12 days. It is also notable that an appreciable decrease in the irreversibly sorbed fraction occurred within the first 5 days. ^[98]

231 Microorganisms, from Cuban soils, were grown in two culture media, using 3,4-DCA, firstly as the sole source of carbon and secondarily as the sole source of carbon and nitrogen. ^[99] The 232 233 pollutant was completely consumed within 3 weeks using *Pseudomonas*, Arthrobacter, 234 Aspergillus, Penicillium, and Fusarium, isolated in the first medium, while Bacillus, 235 Arthrobacter, Cunninghamella, Trichoderma, and Fusarium were isolated in the second system, 236 demonstrating myriad bacterial growth from 3,4-DCA as a feedstock. The biodegradation 237 pathway of 3,4-DCA, and other substituted anilines, involves conversion, by oxygenase, to the 238 corresponding catechol, which is then metabolised via an ortho-cleavage pathway. ^[100] Two 239 modes of dioxygenation have been determined, utilising degrading bacteria obtained by genetic exchange between two strains of Pseudomonas, and leading to the formation of 3- and 4-240 241 chlorocatechol from 3-chloroaniline. In contrast, only 4-chlorocatechol was generated from 242 dioxygenation of 4-chloroaniline.^[94] When bacterial strains of *Pseudomonas* acidovorans were 243 used for the degradation of 3-chloroaniline and 4-choloranaline, the rate-limiting degradation steps were found to be the first attack of the substrate, and conversion to chlorocatechols.^[93] 244

Degradation of 3,4-DCA by *Pseudomonas* sp. showed that catechol 2,3-dioxygenase is integral to process efficiency; ^[95] activity toward 4-methylcatechol, 3-methylcatechol and 4chlorocatechol was found to be 60, 27 and 13%, respectively, of the activity toward catechol 2,3-dioxygenase. Further tests confirmed catechol 2,3-dioxygenase activity using a strain of *Pseudomonas* fluorescens; the presence of 3-chloro-4-hydroxyaniline as a metabolite suggesting
a pathway that includes dehalogenation and hydroxylation of the aromatic ring, followed by ring
cleavage, by catechol 2,3-dioxygenase. ^[96]

Recent work has shown *Micrococcus* sp. to degrade 96% of diuron within 30 hours of incubation, at a concentration of 250 ppm, and with the addition of non-ionic detergent (0.01%). ^[101] The authors proposed a mechanism whereby a methyl group is removed, followed by a hydrolysis step, leading to the accumulation of 3,4-DCA, which undergoes conversion to 4,5dichlorobenzene-1,2-diol, and further intermediates, within 24 hours of test commencement (Fig. 1). Diuron mineralization has also been confirmed by the metabolic cooperation of *Arthrobacter* sp. and *Achromobacter* sp., with CO₂ as the only final product. ^[102]



Figure 1. Degradation pathway of diuron by *Micrococcus* sp, confirmed by FTIR spectra and
 HPLC ^[101]

262 Strains of Aquaspirillum itersonii, Aquaspirillum sp. and Paracoccus denitrificans were shown to successfully use 3.4-DCA as the only source of carbon and nitrogen for growth; ^[103] the latter 263 264 was able to metabolize the pollutant at concentrations up to 150 mg L^{-1} , through oxidation to odiphenol, intradiol cleavage of 4,5- dichloropyrocatechol, and further stages of preparatory 265 266 metabolism associated with dehalogenation. A study of microorganisms isolated from Cuban soils, treated with propanide, showed a Paracoccus denitrificans strain to be most efficacious for 267 268 3,4-DCA ^[50] degradation. The cleavage of the aromatic ring via the ortho- or meta-pathways, following formation of 4,5- dichloropyrocatechol, allows full decomposition. Successful 269 270 adsorptive bioremediation was demonstrated with the introduction of activated carbons and bacteria to polluted soils. ^[104] Activated carbon acts as buffer, which keeps the pollutant 271 272 concentration in the soil solution below the toxicity threshold for the bacteria, as shown by a 273 study of three types of activated carbon saturated with 3,4-DCA and placed in a mineral medium with a Paracoccus denitrificans strain. ^[50] The pollutant was reversibly sorbed, therefore 274 275 available, at a limited concentration, for the bacteria population to process. Varied degradation 276 rates, from 2 to 10 weeks, suggest that facile desorption and more rapid decomposition are 277 linked to a reduced micropore volume. This can be ascribed to the fact that Paracoccus 278 denitrificans is only able to penetrate into the macroporous structure, due to size exclusion 279 effects, thus pollutant desorption from the smaller carbon pores is necessary for the bacteria to 280 process any 3.4-DCA sorbed therein; this bacterium seems able to accelerate desorption by 281 acidifying the medium or via excretion of surface-active substances.

Biological studies have also shown microbial consortia to be successful in the removal of propanil and 3,4-DCA from repeated batch suspended cell cultures, ^[105] as well as in biofilm reactors for agricultural wastewater treatment. ^[106] In the latter case, the porous volcanic stone tezontle was used as a support for a biofilm in a continuous process able to degrade propanil and metabolic intermediates at rates of up to 24.9 mg L⁻¹ h⁻¹, without the need for co-substrates. 287 Pseudomonas sp., Acinetobacter calcoaceticus, Rhodococcus sp., Xanthomonas sp. and Kokuria 288 strains can also grow individually in 3.4-DCA, while other strains found in the biofilm, not able 289 to degrade propanil metabolites directly, are probably involved in the metabolization of 290 herbicide adjuvants or in the maintenance of biofilm integrity. Resultantly, the removal of 291 chloroanilines from sewage treatment plant streams could be improved by promoting the growth 292 of indigenous bacterial communities, and through the introduction of adapted laboratory strains. 293 The addition of readily degradable aniline and non-toxic haloaromatics may, respectively, improve the breakdown of chloroanilines and the chlorocatechol potential.^[94] 294

295 *Uptake by fungi and cultivated plants*

296 When free chloroanilines are released as herbicide metabolites, they can be incorporated in the 297 plant's 'insoluble' residue fraction; degradation experiments have proposed lignin as a primary binding site. ^[107, 108] Immersion of the bivalve *Corbicula fluminea* in cages both upstream and 298 downstream of conventional rice fields, in the region of Camargue, ^[19] showed the concentration 299 300 of 3,4-DCA measured downstream of the rice plantations to be approximately half that in the 301 Corbicula caged upstream, suggesting a potential, partial bioaccumulation of 3,4-DCA in rice 302 plants. Tomato plants, oat, barley and wheat, grown in nutrient solutions with 4-chloroanaline 303 and 3,4-DCA showed that 90-95% of the chloroanilines incorporated were found in the roots, 304 with uptake proportional to the amount of chemical applied. In contrast, distribution of the same 305 chemicals in carrots was approximately equally divided between the roots and the upper part of the vegetables. ^[109] These results suggest a potential risk of chronic toxicity due to the 306 307 assumption of 3,4-DCA contained in certain foods.

Some lignin degraders are able to metabolize chloroanilines and their lignin conjugates;
experiments have shown that chloroanilines appear to be bioavailable to the white rot fungus *Phanerochaete chrysosporium* once they were mineralized as lignin. ^[110] More than 50% of

available [ring-U- 14C] -3,4-DCA was shown to be mineralized after 33 days of sample incubation and free 3,4-DCA was deemed a superior substrate for mineralization than free 4- chloroanaline. Different metabolites were formed, but chloroanilines were not detected, neither were their azo or azoxy derivatives. Hence, lignin incorporation and fungal oxidation can lead to the complete removal of 3,4-DCA from the environment; however, fungi is also known to adsorb less chloro-substituted anilines per biomass unit than bacteria, ^[111] and the degradation pathway of white-rot fungi could lead to the formation of toxic tetrachloroazobenzenes. ^[112]

318 Adsorption and ligand exchange

Adsorption technologies offer effective removal of many organic pollutants from aqueous media, $^{[113]}$ and various adsorbents have been studied for removal of chloroanilines from wastewaters. Batch adsorption experiments, conducted with an acid activated halloysite, using aqueous solutions at pH ~5, $^{[12]}$ gave experimental data that followed a pseudo-second order kinetic model: $^{[114]}$

$$\frac{t}{q_t} = \frac{1}{(k_2 q_e^2)} + \frac{1}{q_e t}$$
(2)

where: q_t is the amount of chloroaniline adsorbed (mg g⁻¹) at time t (s), k_2 is the rate constant of pseudo-second order adsorption (g mg⁻¹ min⁻¹) and q_e is the amount of chloroaniline adsorbed at equilibrium (mg g⁻¹). A 'Weber–Morris' plot of q_t versus $t^{0.5}$ confirmed that chloroaniline removal occurred, first by fast diffusion of 3,4-DCA to the surface of the clay mineral, over the first 180 minutes, before continuing as slower interparticle diffusion. The adsorption capacity of halloysite was found to be lower for 3,4-DCA than for 3-dichloroaniline and 4-dichloroanaline.

330 Equilibrium isotherm data was effectively described by the semi-empirical Langmuir equation:

$$\frac{C_e}{q_e} = \frac{1}{(K_L q_m)} + \frac{C_e}{q_m} \tag{3}$$

where: q_m is the monolayer adsorption capacity (mg g⁻¹), q_e is the sorption uptake at equilibrium 331 (mg g⁻¹), C_e is the equilibrium solution concentration (mg L⁻¹) and K_L is a coefficient related to 332 the affinity between the adsorbent and the adsorbate $(L g^{-1})$. Similar adsorption experiments 333 334 have been performed with kaolinite (KGa-1) and montmorillonite (SWy-1), using standard solutions of 3,4-DCA and other chloroanilines at pH ~5 and ~9, respectively; ^[1, 75] the specific 335 336 pH conditions were chosen so as to produce neutral organic pollutant species. Kinetic 337 evaluation indicated an initial, rapid surge in chloroaniline removal, with equilibrium achieved in under 4 days. Langmuir and Freundlich equations both adequately described the data; ^[75] 338 however, the Langmuir plot showed a marginally better fit for montmorillonite, hence 339 340 adsorption on this clay is likely to decrease as surface sorption sites are saturated. The 341 chloroanilines studied would be mainly sorbed on the mineral surface of kaolinite, while the structure of montmorillonite allows swelling via sorption in the interlayer, ^[115] as confirmed by 342 studying the dehydrated clay; ^[1] post heat-treatment, the distance between equivalent atomic 343 344 planes (d₀₀₁) collapsed from 11 to 9.7 Å. Further evidence was provided by X-ray spectra of the 345 montmorillonite/3,4-DCA system. This contrast in sorption mechanism is reflected in 346 desorption measurements, where kaolinite was shown to retain the pollutant, while 347 montmorillonite showed a higher level of desorption when reversing the sorption process at an earlier point in the isotherm.^[75] 348

While clay materials offer surface sites for adsorption, the main surface area of another wellknown family of sorbents, i.e. activated carbons, is ascribed to microporous character; surface hydrophobicity determines the sorptive capacity of many organic molecules, which have molecular sizes small enough to penetrate into the micropores. Highly microporous activated carbons, obtained from coal and peat, were confirmed as better sorbents than mesoporous carbons, obtained from raw plant materials. Increased iron content and other ash elements may positively influence the maximum uptake, by enhancing chemisorption of active organic
compounds, such as 3,4-DCA. ^[50]

Studies of aqueous solutions of various pesticides agitated with 10 mg L⁻¹ of powdered activated carbon (surface area ~1000 m² g⁻¹; particle size 40 μ m) for 5 minutes, showed 70% removal efficiency for 3,4-DCA (initial concentration: 658 ng L⁻¹), while complete removal was achieved via preoxidation with ozone. ^[103] Fitting of room temperature sorption isotherms, obtained using suspensions of activated carbon in aqueous solutions of 3,4-DCA, ^[50] using the Langmuir isotherm model (Equation 3), showed monolayer filling of the sorptive surface with 'L-type' isotherms, indicating strong interactions between the adsorbate and adsorbent. ^[116]

Sugar beet pulp, corncob, corncob char, perlite, vermiculite and sand have recently been studied 364 for sorption of 3,4-DCA from aqueous solutions at pH 4.8. ^[85] These sorbents may be used in 365 field conditions, so it is essential to understand their sorption behaviour in different matrices. 366 367 However, liquid matrices containing cations and organic matter, except for corncob, showed no 368 significant differences in maximum uptake of 3,4-DCA from pure water and run-off waters. 369 The mechanism of sorption was satisfactorily described by the Freundlich isotherm model, with 370 the highest sorption uptakes obtained at 99% removal from water for corncob char, and, 86% 371 removal for sand. Of the sorbents studied, it is also known that vermiculite has a good resistance to mechanical abrasion. ^[117] Further investigations would be required to verify the 372 373 adsorption capacity of low cost materials in field conditions, but it is encouraging that sorbents 374 such as sand could present appreciable capacities capable of removing > 50% of 3,4-DCA, even 375 from sediment extract media (Table 2).

Table 2. Surface area, pore size and adsorption data of different material tested for the removal
of 3,4-DCA from water. The parameters q_m and b refer to the Langmuir model (Equation 3)

	Surface	Pore			Equilibrium	
			q_m	b		Q.: · 1 _ 1
Adsorbent	area	volume	((T	time	Stirring method
	$(m^2 \sigma^{-1})$	$(am^3 a^{-1})$	$(mg g^{-1})$	$(mL mg^{+})$	(b)	
	(mg)	(cm g)			(11)	
Halloysite ^[12]	76.6	0.039	0.078	2.726	> 3	Rotary stirrer
Kaolinite ^[75]	-	-	0.311	9	> 96	Electromagneti
						_
						с
Montmorillonit	_	_	0.077	23	> 96	Electromagneti
						8
e ^[75]						с
Activated	963	0.55	583	-	48	-
$arbon \Lambda G$ [50]						
carbon AO · ·						
Activated	1028	0.53	480	-	0.5	-
carbon SKT ^[50]						
	110		2.54			
Activated	410	0.5	364	-	0.5	-
carbon RS ^[50]						

378 Within ligand exchange processes, polymeric chelating resins are able to selectively remove 379 target contaminants; however, eluate recycle, regeneration of depleted adsorbent, and the high 380 cost of transition metals, used as ligand complexing ions, are still significant obstacles towards 381 commercial application of such processes in wastewater treatment. Currently, there are no 382 studies on the application of ligand exchange processes for 3,4-DCA removal, but this would 383 seem possible in light of the recovery of aromatic amines from water, at low concentration, as demonstrated for chelating resin-bound cobalt ions. ^[118] A mini-column apparatus with Co(II)-384 385 CDAE-sporopollenin resin was also tested for adsorption of chlorinated anilines, found to be 386 described by a Langmuir model for 2-chloroaniline, 4-chloroaniline and 2,5-dichloroaniline.^[6] The study showed similar values for the maximum adsorption capacity (q_m) for binding of 2-387

388 chloroanilines and 4-chloroanilines, which were consistently lower than those for 3dichloroaniline and 2,5-dichloroaniline onto the Co^{2+} matrix, suggesting that both electrical 389 390 forces and steric hindrance are involved in the sorption process. This conclusion is supported by 391 consideration of the inductive effects of ortho-Cl and para-Cl atoms, as well as the nature of 392 these ligands, which contain charged groups and may offer steric hindrance. Moreover, steric 393 hindrance around the amino nitrogen weakens binding to metal ions, causing faster migration of the aforementioned pollutants. ^[119] The adsorption of 3-chloroaniline was better represented by 394 a Freundlich model, possibly as a result of a more complex type of binding than the independent 395 396 and univalent binding described by a Langmuir model.

397 Chlorination, ozonisation, chemical precipitation and Fe^{θ}/H_2O_2 systems

398 A common sequence of operations adopted in many drinking water plants is that of (i) 399 preoxidation, (ii) adsorption, and (iii) coagulation. Preoxidation of an aqueous sample with a concentration of 658 ng L⁻¹ of 3,4-DCA, performed using sodium hypochlorite, demonstrated 400 100% pollutant removal; ^[13] however, such treatments have an associated risk of carcinogenic 401 402 trihalomethanes by-product formation. Hence, researchers have considered other oxidative species and ozonolysis of a sample, again with a concentration of 658 ng L^{-1} of 3,4-DCA, 403 404 showed 85% pollutant removal; however, the subsequent coagulation and flocculation steps 405 were found to be ineffective, while further adsorption treatment, with activated carbons, led to complete pollutant removal.^[13] 406

The oxidizing potential of Fe⁰ towards different organic compounds is well known; ^[120] Fe⁰/ H₂O₂ systems can be used to reduce levels of diuron, and other pesticides, in polluted environments, as well as agricultural waste. Fe⁰ promotes the reduction of H₂O₂ to hydroxyl radicals, generating Fe²⁺, which, in turn, also produces hydroxyl radicals via further H₂O₂ reduction. A 10 mg L⁻¹ diuron solution, also containing 2 mmol L⁻¹ of H₂O₂ and H₃PO₄, was 412 flowed through a glass tube packed with 2 g of iron wool, and showed that pH strongly affected 413 the degradation process, allowing process optimisation. At pH 2.5 more than 99.9% of the 414 pesticide was removed after ten minutes, with only 1 μ g L⁻¹ of 3,4-DCA found remaining in the 415 effluent. ^[121]

416 Electrochemical and electrohydraulic methods

An electrohydraulic discharge (EHD) method for the oxidative degradation of 3,4-DCA was
tested by exposing wastewaters to pulsed electrical discharges generated via submerged
electrodes. ^[122] UV radiation is produced by a plasma channel created by EHD, thereby,
generating a shockwave as it expands against the water. The degradation rate is expressed by:

$$\frac{dC}{dN} = -k_1 C_i - k_0 \tag{4}$$

421 where dC/dN is the change in concentration per discharge, C_i is the initial substrate 422 concentration, k_0 is the zero-order term (an expression of direct photolysis) and k_1 is the first-423 order term related to oxidation in the plasma channel region.

424 As part of an Advanced Oxidation Process (AOP), photocatalysis can be employed (i) for water 425 treatment in slurry reactors, where an additional step is required for the separation of any 426 suspended catalysts, or (ii) into reactors, where the catalysts are immobilized on adsorbents or 427 on membranes. Using sols of vanadium pentoxide and cerium oxide, added to a titanium dioxide sol, allowed preparation of Ti–V and Ti–Ce catalysts, respectively: 0.1 g L^{-1} of each 428 429 powdered catalyst was added to agitated aqueous solutions of 3,4-DCA, irradiated in an annular reactor at 140 mW cm⁻², and the Ti–V catalyst gave a higher degradation than Ti-Ce, due to its 430 431 band gap energy (which is more towards the visible region) and smaller particle size. The 432 kinetic plot suggested bi-phasic kinetics, with a sharp increase in rate after 45 minutes; further bench scale reactor experiments showed 85% degradation in 106 minutes ^[11] and Figure 2 shows
the intermediate species formed.



Figure 2. Intermediates formed during photo-degradation of 3,4-DCA using Ti-V (sol) catalyst,
confirmed by HPLC and GC-MS analysis ^[11]

435

Biphasic kinetics were also observed in the photocatalytic degradation of 3,4-DCA using Ti-N 438 and Ti-S catalysts; ^[28] the former showing a higher surface area, and lower particle size and 439 band-gap energy. Higher specific surface area increases the degree of contact of the pollutant 440 441 with the catalyst surface, while smaller particle size means a reduced degradation time, due to 442 shorter distances between the charge carrier and the surface, where the reaction occurs. 3,4-443 DCA was fully degraded using a Ti-N catalyst in 120 minutes with optimal degradation 444 obtained at pH = 6. At higher catalyst dosages (> 0.1 g L^{-1}) the reaction rate starts to decrease, due to the deactivation of molecules that collide with ground state molecules, and subsequent 445 agglomeration of catalyst particles. Meanwhile, at 3,4-DCA concentrations $> 10 \text{ mg L}^{-1}$, the 446 447 degradation efficiency starts to decrease, as the number of collisions between the 3,4-DCA

448 molecules increases, while there is a reduction in collisions between pollutant molecules and
449 •OH radicals.^[123]

450 Degradation of aqueous 3,4-DCA was recently performed using a dielectric barrier discharge (DBD) plasma reactor; ^[124] where generated ozone interacts with the pollutant directly or by the 451 generation of hydroxyl radicals, which results in a faster rate of reaction than for molecular 452 453 ozone alone. ^[125] The process involves the flow of a water film through the discharge zone 454 created by two aluminium electrodes, and the degradation process is well described by pseudo-455 first order kinetics, with higher efficiencies reached either under acidic conditions, increasing the input power or by adding Fe^{2+} or Fe^{3+} . The main pathways involved were deamination, 456 457 hydroxylation, dechlorination, and hydroxylation and oxidation, followed by the generation of organic acids, via aromatic ring opening. Mineralization into CO₂ and H₂O was only partially 458 459 achieved, as confirmed by the lower rate of removal for total organic carbon than for DCA, and 460 by degradation intermediates identified using GC-MS analysis. Solution pH decreased during DCA degradation, as observed in previous work, ^[124] where aqueous 3,4-DCA was degraded by 461 462 a wire-cylinder DBD reactor, with an efficiency that was observed to increase when the input 463 power was increased to 90 W, but decreased at powers above that; aqueous ozone concentration 464 was seen to follow the same trend. It was also noted that, similar to other systems, the process 465 was pH dependent with a lower degradation rate obtained under neutral conditions than at acidic 466 or basic levels.

467 Conclusions

Myriad technologies have been developed for the degradation of pesticides; however, more attention has to be mainly focussed on the fate of metabolites. 3,4-DCA is a degradation product generally more toxic than its parent substances; if it is covalently bound to humic 471 substances within soil, the risk of groundwater contamination via leaching is low, but it also has
472 an extremely low rate of mineralization, ^[70] making it a significant environmental issue.

473 Lignin incorporation and fungal oxidation are able to effect complete removal of 3,4-DCA from the environment, ^[110] while the use of bacteria and porous materials can be successful in 474 475 bioreactors, as well as for in-situ bioremediation techniques. Bioremediation has been successfully demonstrated, introducing activated carbons and bacteria to polluted soils. ^[50] and 476 477 the biological removal of 3,4-DCA from sewage can be enhanced by the growth of indigenous communities, and through the introduction of adapted laboratory strains; ^[94] however, the 478 479 technical and economic feasibility of such processes also need to be considered. Further 480 investigations are required to confirm the adsorption capacity of promising low cost materials 481 such as activated carbons, corncob char and sand, especially within field conditions.^[85] The 482 possibility of recovering aromatic amines from low concentration water streams has been already demonstrated using chelating resin-bound cobalt ions, ^[118] as well as for Co(II)-CDAE-483 sporopollenin resin, ^[6] but there have been no specific studies related to the application of such 484 485 technologies to 3,4-DCA removal.

Fe⁰/H₂O₂ systems could be developed for the degradation of 3,4-DCA in agricultural soils and waste, ^[121] while photodegradation using doped TiO₂ has been successfully performed, and degradation kinetics are available for the scale up of reactors. ^[11] Low toxicity and cost, combined with good chemical stability and high natural abundance ^[126] make this catalyst potentially suitable for the environmentally friendly removal of 3,4-DCA from water. Effective degradation is also observed for the use of dielectric barrier discharge reactors, but further studies are required to reach complete mineralization of 3,4-DCA. ^[124]

Hence, there is significant scope for the application of existing technologies to the issue of 3,4-DCA removal from aqueous streams, some of which have timely potential for implementation;

- 495 however, there is a need for more data to be acquired to permit economic and environmental
- 496 impact of these proposed systems to be fully addressed.

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 General. 2008, 340(2), 153-161.

847 Figures and Tables

- 848 Figures and tables are listed below.
- 849 Table 1. Properties of 3,4-dichloroaniline

Property	Value	Ref.	
Molecular formula	C ₆ H ₅ Cl ₂ N	-	
Molecular structure	CI NH2	[15]	
Appearance	Solid at 293 K	[15]	
Molecular weight	162 g mol ⁻¹	[15]	
Molecular size	0.35 nm ²	[50]	
Henry's constant	0.05 Pa m ³ mol ⁻¹	[15]	
Solubility in water	580 mg L ⁻¹ at 293 K	[15]	
Octanol-water partition coefficient (log Kow)	2.7 (shaken flask method)	[5, 16]	
Estimated surface water half life	18 days	[15]	
Measured rate of loss from outdoor water systems	0.11 - 0.17 day ⁻¹	[4]	
	0.06 - 0.14 day ⁻¹	[49]	
Estimated atmospheric half life	9 hours	[15]	
Estimated half-life in soil and sediment	470 - 1500 days	[51]	



Figure 1. Degradation pathway of diuron by *Micrococcus* sp, confirmed by FTIR spectra and
HPLC ^[101]

Table 2. Surface area, pore size and adsorption data of different material tested for the removal of 3,4-DCA from water. The parameters q_m and b refer to the Langmuir model (Equation 3)

	Surface	Pore			Equilibrium	
Adsorbent	area	volume	q_m (mg g ⁻¹)	<i>b</i> (mL mg ⁻¹)	time	Stirring method
	$(m^2 g^{-1})$	$(cm^3 g^{-1})$			(h)	
Halloysite ^[12]	76.6	0.039	0.078	2.726	> 3	Rotary stirrer
Kaolinite ^[75]	-	-	0.311	9	> 96	Electromagneti
						с
Montmorillonit	-	-	0.077	23	> 96	Electromagneti
e ^[75]						С
Activated	963	0.55	583	-	48	-

carbon AG ^[50]						
Activated	1028	0.53	480	-	0.5	-
carbon SKT ^[50]						
Activated	410	0.5	364	-	0.5	-
carbon RS ^[50]						



Figure 2. Intermediates formed during photo-degradation of 3,4-DCA using Ti-V (sol) catalyst,

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860 confirmed by HPLC and GC-MS analysis <sup>[11]</sup>
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